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Table 1: MIC Storage System Hazard Analysis	CREDIT		Credit taken after applying the LOPA "Independent Protective Layer" (IPL) rule.
	(probability of failure, in years)		
Initiating Event [IE] or Safeguard [SAF] Description	Available	Taken	Explanation
[IE] E-213 MRS Condenser cooling water leak into MIC Storage Tank	1/100	1/10	Conservative credit (1/10) taken: History of leaks in existing process
[IE] MIC Circulation Pump Failure (multiple failures per year)	1/10	1 (no credit)	11 °C high temperature alarm stays active until the pump is repaired
[SAF] Refrigeration Unit	1/10	1 (no credit)	No IPL: Common Mode Failure - requires a working Circulation Pump
[SAF] High MIC Temperature Alarm + Procedure to isolate tank	1/10	1 (no credit)	No IPL: Circulation Pump, alarm integrity, and operator dependencies
[SAF] High MIC Temperature Alarm + MIC Unit transfer (reprocessing)	1/10	1 (no credit)	No IPL: Circulation Pump, alarm integrity, and operator dependencies
[SAF] High MIC Temperature Alarm + E-611 transfer (quench)	1/10	1 (no credit)	No IPL: Circulation Pump, alarm integrity, and operator dependencies
[SAF] High MIC Temperature Alarm + E-619 transfer (more cooling)	1/10	1 (no credit)	No IPL: Circulation Pump, alarm integrity, and operator dependencies
[SAF] High MIC Temperature Alarm + VGS transfer (destruction)	1/10	1 (no credit)	No IPL: Circulation Pump, alarm integrity, and operator dependencies
[SAF] High MIC Temperature Alarm + Solvent quench	1/10	1 (no credit)	No IPL: Alarm already active ("Common Trouble" when pump fails)
[SAF] Independent control room temperature gauge + Solvent quench	1/10	1 (no credit)	Undetectable ("Common Trouble" when pump fails - see Figure 3)
[SAF] Vent Valve automatically opens (Basic Process Control System)	1/10	1 (no credit)	Choked vapor flow through vent during a thermal runaway reaction
[SAF] Safety valve opens when tank pressure reaches 40 PSIG	1/100	1 (no credit)	Take credit only after VGS/Flare load calculations confirm capacity
Frequency of Consequence:	1 x 10 ⁻¹⁴	1 x 10 ⁻¹	Taking credit only for safeguards that conform with LOPA rules exposes a credible scenario that is also highly-probable.
Double Jeopardy? Due to design dependencies a MIC Circulation Pump failure would defeat seven safeguards. However, the pump failure is independent from a contamination event that could initiate a thermal runaway reaction. Therefore, this situation may represent a highly-improbable "double jeopardy" scenario. That is not true in this scenario since only one failure is detectable. Without an independent high pressure alarm, only the MIC Circulation Pump failure is detectable and a simultaneous or later contamination event can go unnoticed.			

Designing a system with multiple safeguards may give the impression that an incident is not realistically possible.

MIC STORAGE TANK (Figure 1)

Rising pressure inside the tank would cause the Vent Valve to automatically open, to prevent the internal tank pressure from exceeding 2 PSIG.

FROM HIGH PURITY NITROGEN HEADER

TO RELIEF VALVE VENT HEADER (RVVH)

MIC in the RVVH went to (1) the VGS and (2) the flare if needed.

SAFETY VALVE

Congested flow through the Vent Valve would open the Safety Valve at 40 PSIG to avoid exceeding the tank's Maximum Allowable Working Pressure (MAWP).

CONCRETE DECK

EARTH MOUND

E-610

GROUND LEVEL

NO pressure alarm (indicator and controller only).

PI — PRESSURE INDICATOR
PIC — PRESSURE INDICATOR/CONTROLLER

MIXING EDUCTOR

The Storage Tank could be diluted with excess solvent as a heat sink if an exothermic reaction overloaded the refrigeration unit's capability.

SUMP

TO PROCESS VENT HEADER (PVH)

FROM TRANSFER PUMP RETURN

FROM REFRIGERATION UNIT

FROM MIC REFINING STILL (MRS)

TO DERIVATIVES UNIT

TRANSFER PUMP

CIRCULATION PUMP

REFRIGERATION UNIT

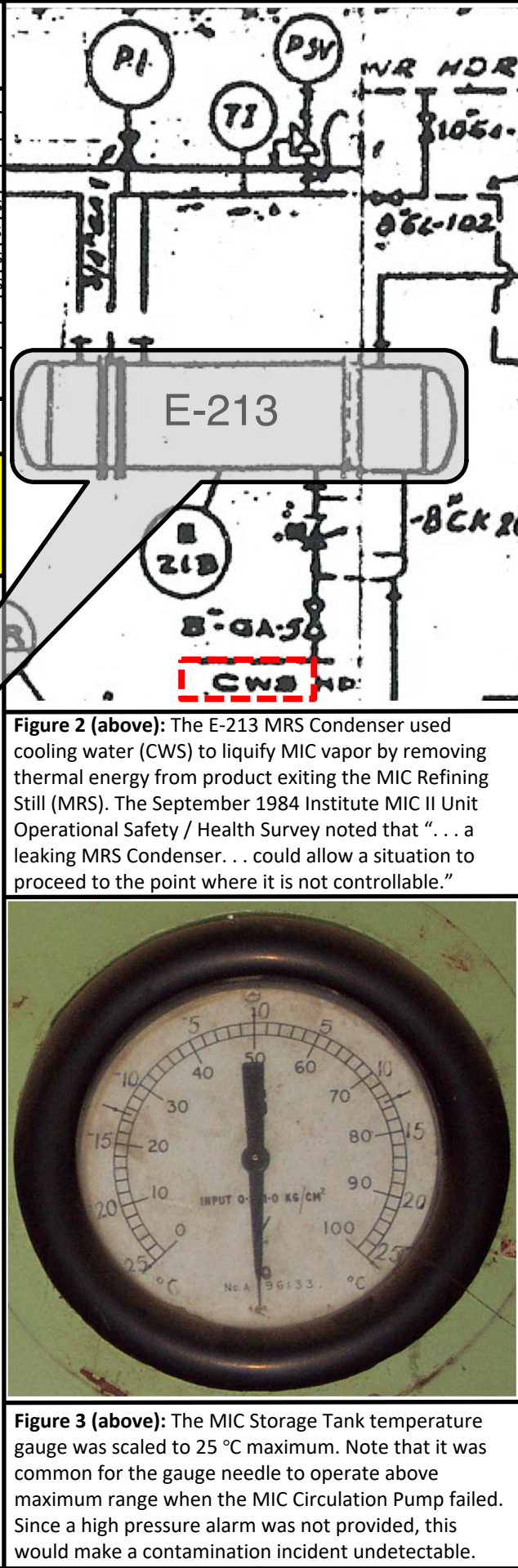
TO REJECT LINE

The Circulation Pump was needed for MIC to enter the Refrigeration Unit and Reject Line.

The Refrigeration Unit removed energy from hot MIC, to slow an exothermic reaction inside the tank.

Contaminated MIC could be routed to the Reject Line for transfer into (1) the MIC Unit, (2) MIC Storage Tank E-611, (3) Reject Tank E-619, or (4) the VGS.

TIA — TEMPERATURE INDICATOR/ALARM
LIA — LEVEL INDICATOR/ALARM



NOTES

Purpose: Use a modern, accepted industry practice to assess the ability for the MIC Storage System in Bhopal India (Figure 1) to operate safely.

Step 1: Establish Risk Tolerance
Risk = Frequency x Consequence. Since 0 risk is unattainable for any industrial process, the goal is to achieve as close to 0 risk as possible. This is done by using system design to minimize the frequency of an event. For a toxic chemical (MIC) release that can produce multiple fatalities, a frequency of 1 event in 10,000,000 years (1 x 10⁻⁷) might be acceptable and achievable. If design allows the frequency of this event to be higher than 1 x 10⁻⁷ years, then the system does not meet safety requirements and must be redesigned.

Step 2: Define a credible scenario
The E-213 MRS Condenser (Figure 2) leaks cooling water into the MIC rundown line, resulting in a thermal runaway reaction inside the MIC storage tank. Tank pressure increases above MAWP (40 PSIG) as the MIC starts to boil, causing the tank to burst; releasing MIC into the atmosphere resulting in multiple inhalation injuries and fatalities.

Step 3: Calculate the "Frequency of Consequence"
Multiplying all allowable credits results in a 1 x 10⁻¹ Frequency of Consequence (see Table 1.)

Step 4: Compare the "Frequency of Consequence" with Risk Tolerance
The Frequency of Consequence (1 x 10⁻¹) is higher than the Risk Tolerance (1 x 10⁻⁷) so a redesign is required.

MIC Storage System Design Drawing obtained from:
<https://tinyurl.com/y3m7w3y5>

